



μ μ

&

&

μμ



16 :



16 :

16.1

16.1.1

$$Re = \frac{V_m h}{\nu}$$

ν : kinematische Viskosität [m²/s],
 μ : dynamische Viskosität [Pa·s],
 ρ : Dichte [kg/m³],
 V_m : mittlere Geschwindigkeit [m/s],
 h : hydraulischer Durchmesser [m].
 Reynolds (laminar) $Re < 2000$, (turbulent) $Re > 4000$.

V_m : [m/s],
 h : [m],
 ν : [m²/s].
 Prandtl ()
 von Karman:

$$\frac{V(y)}{V_c^*} = \frac{1}{K} \ln \frac{y}{k_s} + B \quad (16.1)$$

$V(y)$: [m/s] y [m],
 V_0^* : (shear velocity) [m/s],
 :

von Karman,

$$k_s = 0.4 \frac{\mu}{\rho_w V_0^*} \quad (16.1)$$

V_0^* [m/s] :
 ρ_w [kg/m³].
 (shear stress) [N/m²],

$$V_0^* = \sqrt{\frac{\tau_0}{\rho_w}} \quad (16.2)$$

τ_0 [N/m²],
 ρ_w [kg/m³].

viscous sublayer), (laminar sublayer
smooth boundary), (hydraulically

$$B = \frac{1}{K} \ln \frac{V_0^* k_s}{\nu} + 5.5, \quad \text{valid } \frac{V_0^* k_s}{\nu} \leq 5 \quad (16.3)$$

rough boundary), (hydraulically

$$B = 8.5, \quad \text{valid } \frac{V_0^* k_s}{\nu} \geq 70 \quad (16.4)$$

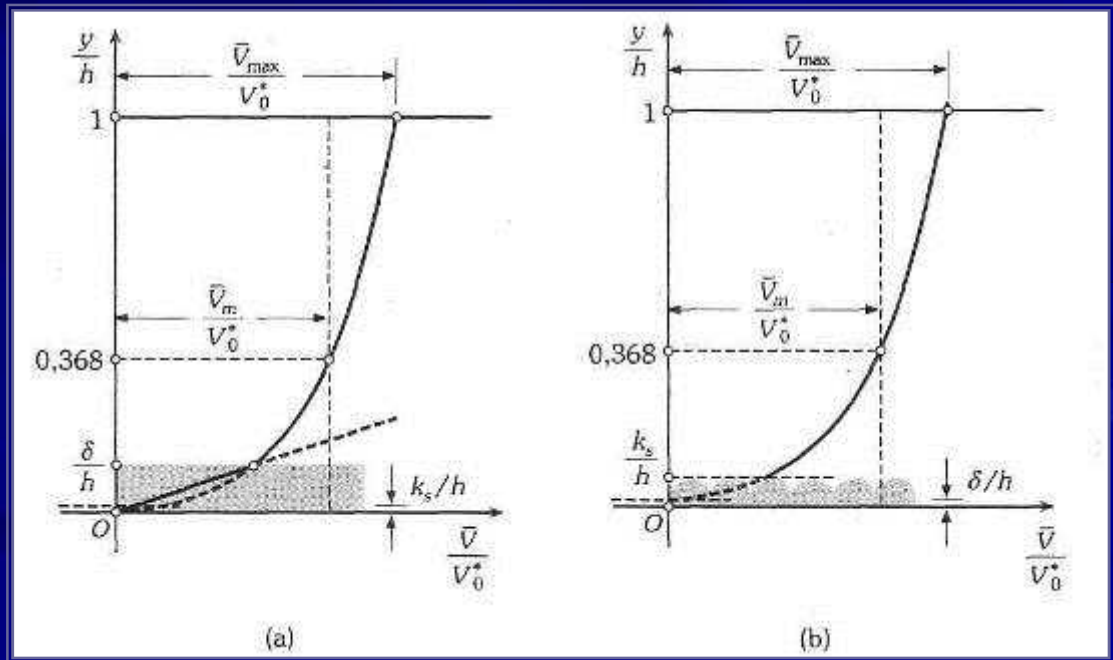
$$\dots (16.1)$$

$$5 < \frac{V_0^* k_s}{\nu} < 70, \quad (16.5)$$

Zanke (1982):

$$B = \left(2.5 \ln \frac{V_0^* k_s}{v} + 5.5 \right) 3.32 \frac{v}{V_0^* k_s} + 8.5 \left(1 - 3.32 \frac{v}{V_0^* k_s} \right) \quad (16.6)$$

$y_m = 0.368 h$ (h : channel depth)



16.1: Velocity profile (Bechteler et al, 1983).

$$\delta = 11.64 \frac{\nu}{V_0^*} \quad (16.7)$$

(16.3)

layer).

μ
 μ μ
 μ

Prandtl

Von Karman μ

μ

$$\frac{V(y)}{V_0^*} = \frac{1}{K} \ln \frac{y}{y'}, \quad (16.8)$$

y' [m]

μ
 μ

$$y' = \frac{\beta V}{V_0^*} \quad (\beta = 0.111), \quad \text{υδραυλικά λείο τοίχωμα} \quad (16.9)$$

$$y' = \gamma k_s \quad (\gamma = 0.0333), \quad \text{υδραυλικά τραχύ τοίχωμα} \quad (16.10)$$

16.8

$V = 0$

$V' = 0,$

$y = y'$

$y/y' = 1.$

$$\frac{V(y)}{V_0^*} = a \left(\frac{y}{y'} \right)^m. \quad (16.11)$$

y' [m]

$V = 0$

μ

μ

(1991).

μ

$V' = 0,$

μ

μ

$y = 0$

μ

μ

$y/y' = 0.$

a

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

μ

(y')

Chen

16.1.2

Darcy-Weisbach:

$$I = f \frac{1}{D} \frac{V_m^2}{2g} \quad (16.12)$$

I : $\mu\mu$ [-],
 f : (),
 D : μ [m],
 V_m : μ [m/s],
 $(V_m = Q/A, Q: [m^3/s], : \mu [m^2]),$
 g : [m/s²].

f , μ μ μ , μ
 Colebrook White:

$$\frac{1}{\sqrt{f}} = -2 \log \left(\frac{2.51}{Re \sqrt{f}} + \frac{k_s/D}{3.72} \right), \quad f = f(Re, k_s/D) \quad (16.13)$$

$k_s = 0$

16.13,

Re

16.12 16.13

o

(

Darcy-Weisbach
R [m]

[m²]
Darcy-Weisbach

Colebrook-White,

D = 4R,

U [m].

$$I = f \frac{1}{4R} \frac{V_m^2}{2g} \quad (16.14)$$

$$f = f(Re, k_s/R, \text{γεωμετρία της διατομής, δομή της τραχύτητας}), \quad (16.15)$$

k_s/R

16.1.3

$\tau_{0,m}$ [N/m²]:

$$\tau_{0,m} = \rho_w g R I \quad (16.16)$$

ρ_w : () [kg/m³],
 g : [m/s²],
 R : [m],
 I : [-].

ρ_w : () [kg/m³],
 g : [m/s²],
 R : [m],
 I : [-].

16.1.4

Colebrook-White,

Darcy-Weisbach

Q , V_m

Manning - Strickler (

Gauckler - Manning),

$$V_m = k_{st} I^{1/2} R^{2/3} \tag{16.17}$$

k_{st} :

R [m], V_m [m/s], k_{st} , n , $1/n$

k_{st}

16.1.5

16.1.2

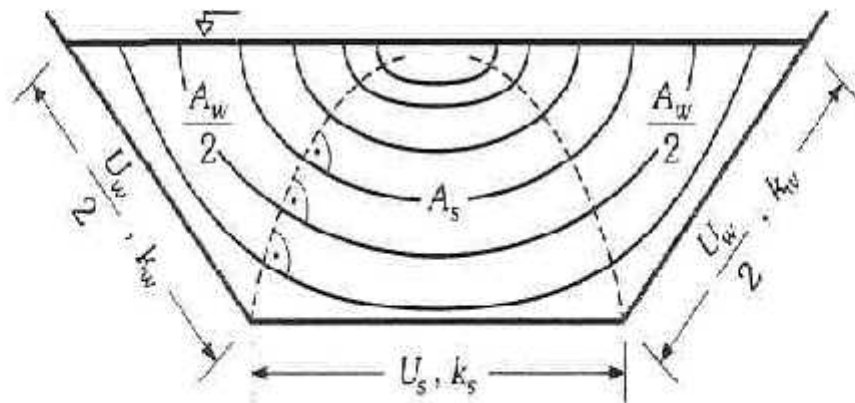
Einstein (1950)

$$\tau_0 = \tau'_0 + \tau''_0 \quad \text{h} \quad f = f' + f'' \quad (16.18)$$

Einstein,

R_s [m] A_s [m²],
 (16.2):

$$R_s = \frac{A_s}{U_s} \quad (16.19)$$



. 16.2: R_s U_s A_s U_w k_w k_s
 (DVWK, 1988).

$U_s[m]$

w

μ

μ

$\cdot 16.2$

$\mu \mu$

μ

μ

μ

$:$

R_s

$$\tau_0 = \rho_w g R_s l$$

(16.20)

f'

μ

$:$

μ

$,$

$$f' = f \left(\frac{V_m R_s}{v}, \frac{R_s}{d_{50}} \right),$$

(16.21)

μ

μ

$($

$,$

$.)$

$,$

$:$

$$f'' = f \left(\frac{V_m}{\sqrt{g d_{50}}}, \frac{R_s}{d_{50}} \right)$$

(16.22)

d_{50}

μ

50%

μ

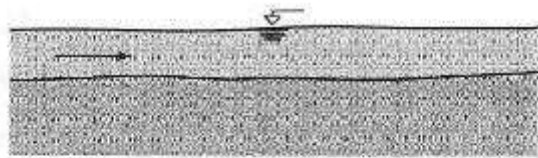
$,$

μ

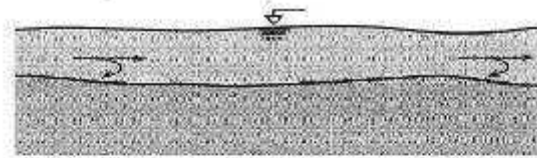
μ

d_{65}, d_{90}

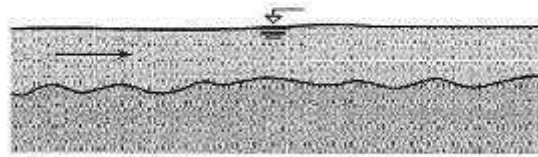
\cdot



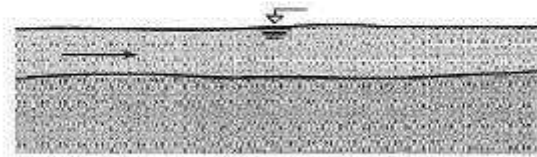
1. Επίπεδος πυθμένας χωρίς μεταφορά $F_r \ll 1$



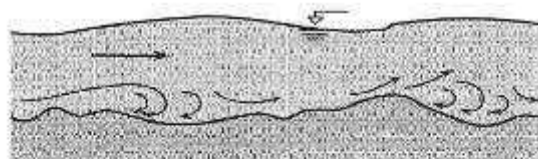
3c. Μετάβαση από δίνες σε επίπεδο πυθμένα, $F_r < 1$



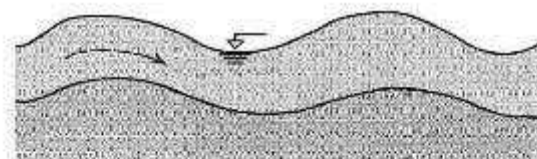
2. Ρυτίδες, $F_r \ll 1$ και $d_m < 0,5 \text{ mm}$



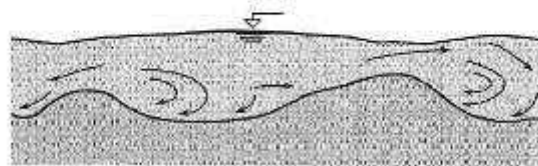
4. Επίπεδος πυθμένας με μεταφορά $F_r < 1$



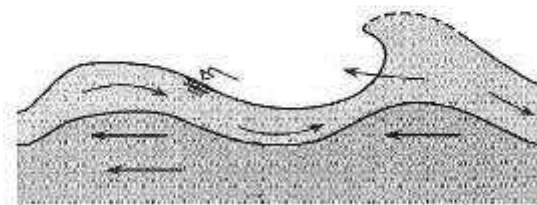
3a. Δίνες με ρυτίδες, $F_r \ll 1$ και $d_m < 0,5 \text{ mm}$



5. Στάσιμα κόματα, $F_r \gg 1$



3b. Δίνες, $F_r < 1$



6. Αντιδίνες $F_r > 1$

.16.3: μ μ μ μ

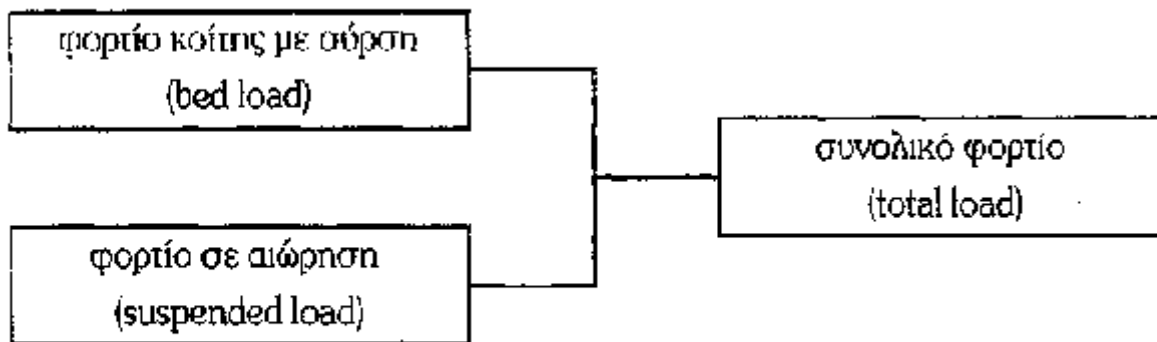
(μ Froude Fr < 1), 1, 2, 3, 3b, μ 4, 5, 6
 (Fr > 1). 3c (Fr = 0.61.2)

. 16.3,

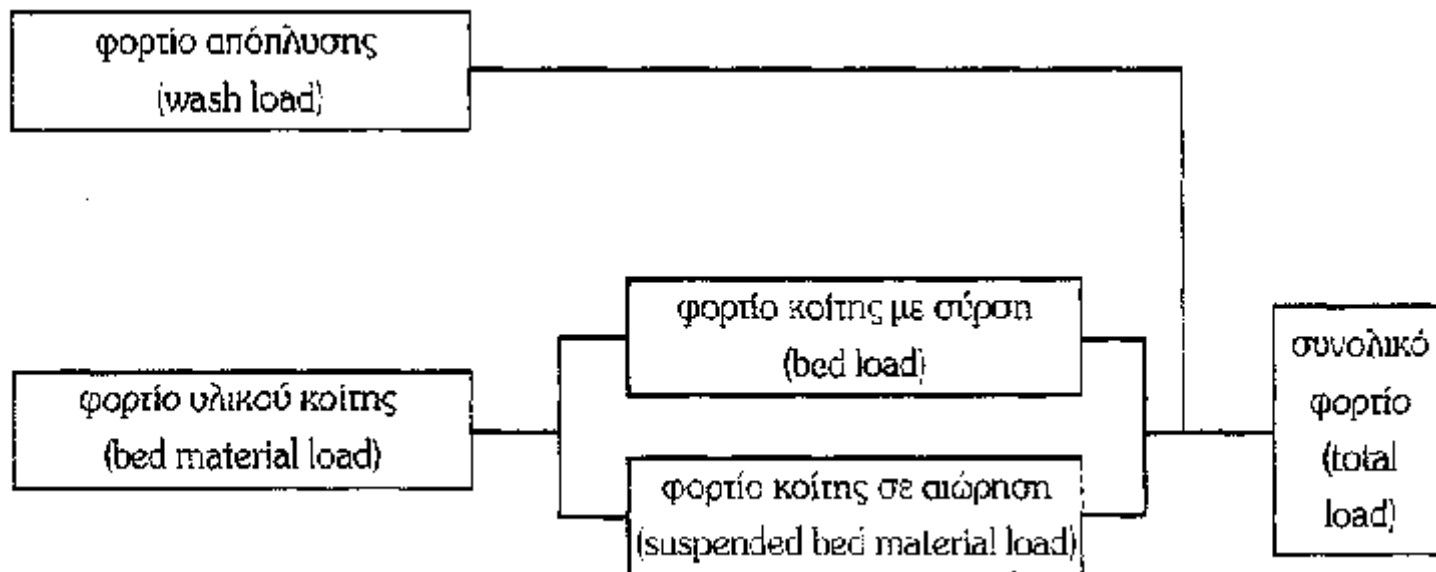
16.2

μ
 16.4).

Διάκριση σύμφωνα με τον τρόπο μεταφοράς



Διάκριση σύμφωνα με τη σχέση των φερτών υλικών προς την κοίτη



χ. 16.4:

(Vetter, 1992)

μ (bed load) μ
 μ , μ
 (suspended load) μ
 μ μ
 (bed material load) μ μ
 μ μ . 16.4
 (wash load) μ μ
 μ μ
 μ 0.062 mm (μ)
 μ μ μ
) μ μ μ
 (suspended load) μ (bed load) μ Froude:

$$F_r^2 = \frac{V_m^2}{gd} = 360 \quad (\text{Kresser, 1964}) \quad (16.23)$$

V_s

:

$$\frac{V_s}{K V_0^*} = 10,$$

(Engelund, 1965)

(16.24)

Von. Karman (0.4).

16.3

μ μ μ μ μ μ μ μ μ μ [kg/s] [N/s] [m³/s].

$$\left[\frac{\text{kg}}{\text{s} \cdot \text{m}} \right] \dot{h} + \left[\frac{\text{N}}{\text{s} \cdot \text{m}} \right] \dot{h} = \left[\frac{\text{m}^3}{\text{s} \cdot \text{m}} \right] \dot{h}$$

(bed load), (total load), (suspended load)

(, 1985)

μ . . . [kg/m³].

16.3.2

A wastewater treatment plant receives influent with a BOD concentration of 100 mg/l and a flow rate of $1 \text{ m}^3/\text{s}$. The plant has a detention time of 30 m . The effluent is discharged into a river with a flow rate of 5 ltr/s . The river has a flow velocity of 0.8 h , 0.4 h , 0.2 h , and 0.05 h . The decay constant is $1/6$ and $1/10$. The concentration of BOD in the river is C .

$$C = \frac{\sum C_i Q_i}{\sum Q_i} \quad (16.25)$$

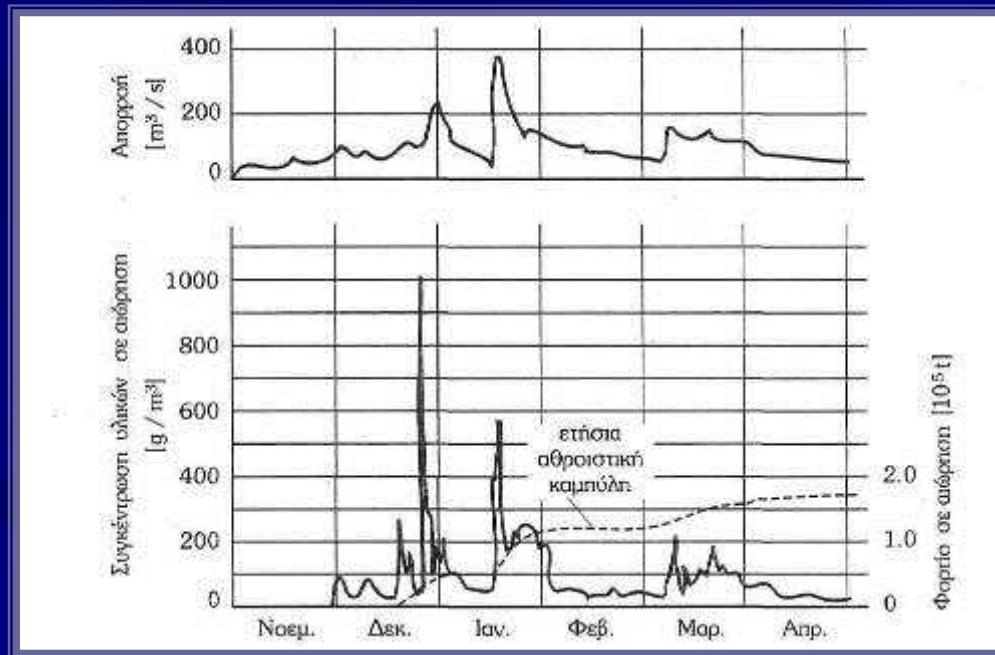
m_s μ

∴

$$m_s = CQ_1 \quad (16.26)$$

 Q μ μ μ b μ $b/10$ μ $\mu \quad b/20.$ μ μ μ μ μ μ μ μ μ μ $\mu\mu$ μ μ μ μ μ $\mu\mu$ μ $\mu\mu$ μ μ μ

16.5
 (Herrenhausen/ Hannover,).
 Leine.
 :



16.5:

" "

(Maniak, 1988).

$$C = aQ^b \quad (16.27)$$

$$m_s = aQ^b \quad (16.28)$$

μ

:

$$\log m_s = a + b \log Q \quad (16.29)$$

μ

μ μ

Greene

(

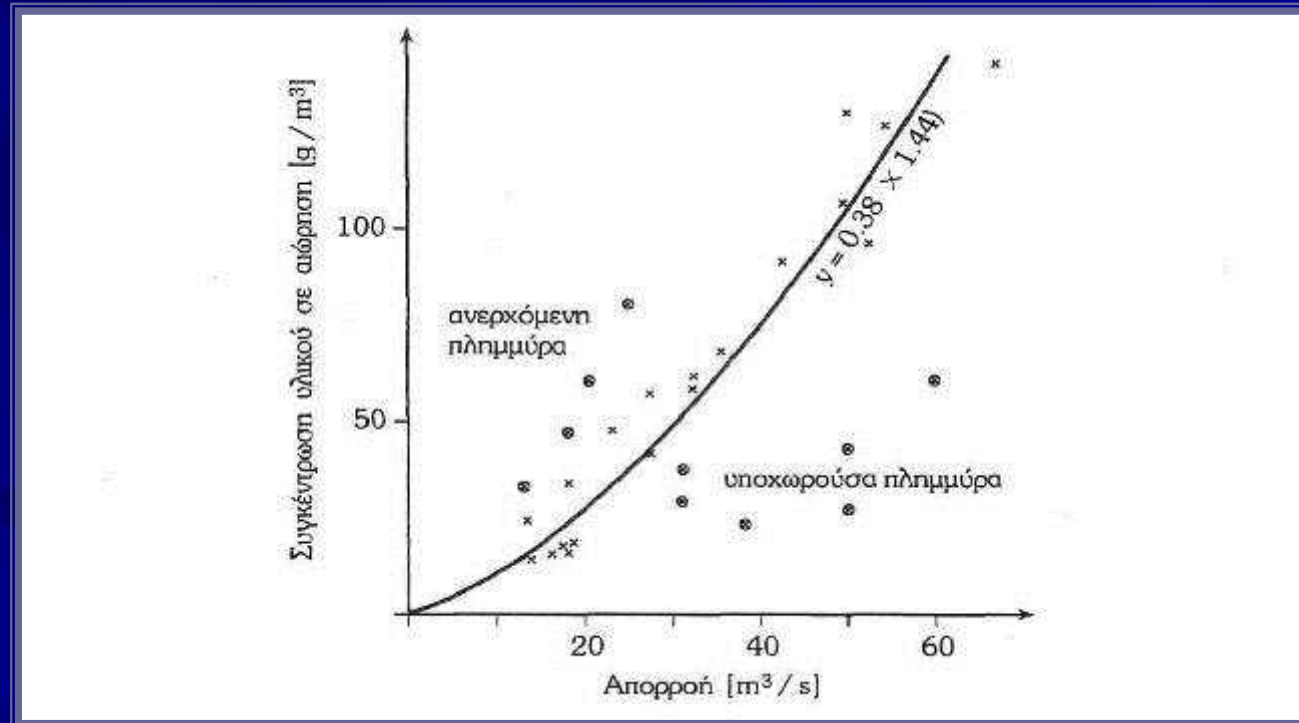
μ Leine (μ)

2916 km²)

. 16.6

. 16.6:

μ μ
μ μ
(Maniak, 1988).



16.4

. 16.2

μ

μ

$(\mu)\mu$

μ

μ

(. 16.7):

- .
- .
- .
- .
- .
- .

μ

$m_G,$

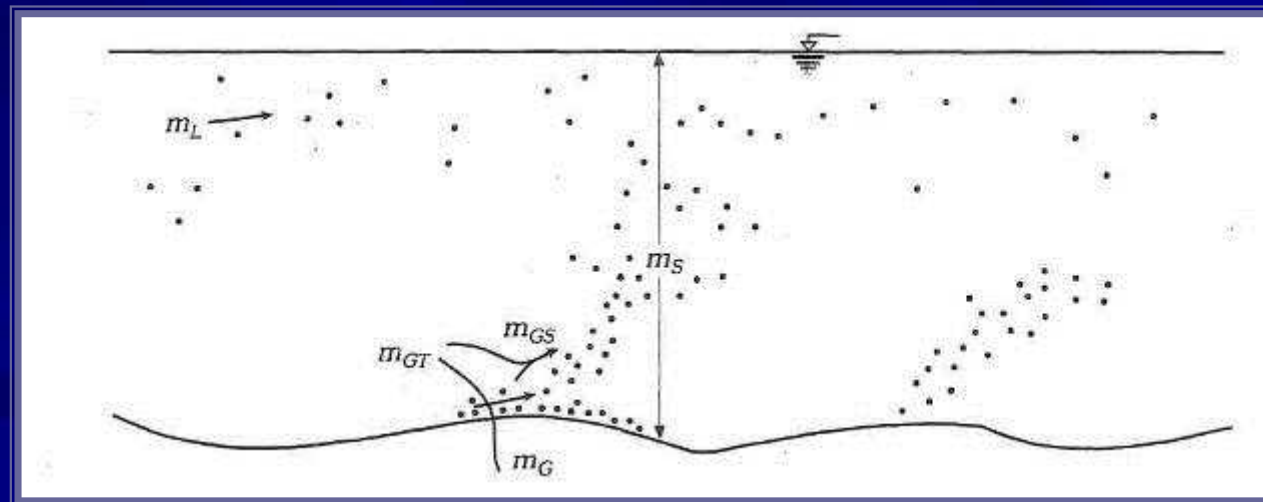
$m_{GS},$

$m_G,$

$m_L,$

$m_S,$

m_P



. 16.7:

μ

μ

:

$$m_{GT} = m_G + m_{GS} \tag{16.30}$$

$$m_S = m_L + m_{GS} \tag{16.31}$$

$$m_F = m_S + m_G = m_L + m_{GT} \tag{16.32}$$

μ

μ

16.1.

μ
 μ
 I.
 II.
 .
 IV, V.

μ
 μ
 m_c
 μ
 m_{GT} (
 μ
 ms (μ
 μ (μ

:

m_{GS}, m_L).
 μ m_{GS} ,
 V.

(IV.

).

VI.

μ m_F (μ

μ m_G, m_{GS}, m_L)

Πρόβλημα	Μέγεθος που χρησιμοποιείται:
(i) Υπολογισμός χρόνου για την πλήρωση με φερτά υλικά ενός χαμηλού προφράγματος (low diversion dam)	m_G
(ii) Υπολογισμός χρόνου για την πλήρωση με φερτά υλικά ενός κανονικού προφράγματος	m_{GT}
(iii) Υπολογισμός νεκρού όγκου ταμιευτήρα	m_{GT} ή m_F
(iv) Σχεδιασμός αντλητικών συγκροτημάτων που χρησιμοποιούν την παροχή του ρεύματος	m_{GS} ή m_{GT}
(v) Σχεδιασμός υδροληψίας από το ρεύμα	m_{GS} ή m_S
(vi) Διευθέτηση υδατορεύματος	m_{GT}
(vii) Σχεδιασμός εγκαταστάσεων επεξεργασίας νερού	m_L
(viii) Μελέτες απομάκρυνσης των φερτών (Dredging)	m_{GT}

load)

μ

(bed load),
(total load).

(suspended

μ

μ

:

1.

μ

μ

μ

μ

(. . $d_m, d_{50}, d_{35}, d_{65}, d_{90}$)

2.

μ

μ

3.

μ

μ

μ

μ

μ

μ

4.

μ

μ

5.

(

μ

)

μ

(bed material load), μ

μ

μ

)

(

,

μ

(

,

μ

μ

(

μ

,

μ

).

,

(wash

load)

μ

,

μ

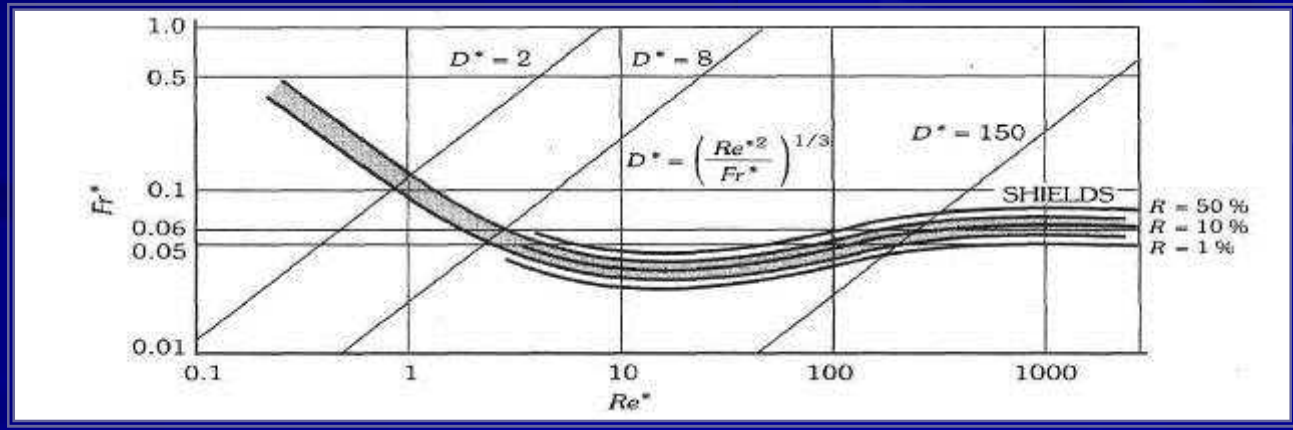
μ

Shields (1936).
 (16.8)

$$\frac{\tau_0}{(\rho_F - \rho_w) g d_{ch}} = f \left(\frac{V_0^* d_{ch}}{\nu} \right) \quad \text{h} \quad F_r^* = f(Re^*) \quad (16.33)$$

τ_0 [N/m²],
 ρ_F [kg/m³],
 ρ_w [kg/m³],
 g [m/s²],
 d_{ch} [m],
 V_0^* [m/s],
 ν [m²/s],
 Re^* Froude,
 Re^* Reynolds

16.8 Shields,
 Zanke (1990)
 (R: " "
 ")



Muller (1949), (Meyer - Peter)

Meyer-Peter Muller (1949)

$$m_G = \frac{8}{g} \frac{\rho_F}{\rho_F - \rho_w} \sqrt{\frac{1}{\rho_w}} (\rho_w g I_R R_s - 0.047 \rho' \rho_w g d_m)^{3/2} \quad (16.34)$$

$$m_G = \frac{8}{g} \frac{\rho_F}{\rho_F - \rho_w} \sqrt{\frac{1}{\rho_w}} (\tau_0 - \tau_{ocr})^{3/2}, \quad (16.35)$$

m_G

[kg/m.s],

$$I_R = \left(\frac{k_{st}}{k_r} \right)^{3/2} I$$

I

[-],

k_{st}

:

Stockier [m^{1/3}/s], (

, . . . 16.17),

$$k_r = \frac{26}{d_{90}^{1/6}}$$

:

[m^{1/3}/s], d₉₀ [m],

$$R_s = h \frac{Q_s}{Q}$$

:

μ μ
[m],

μ

h :

[m],

Q :

μ [m³/s],Q_s :

μ μ

μ

[m³/s],

$$d_m = \frac{\sum d_i \Delta p}{100}$$

: μ

μ

[m],

 d_i

:

μ

μ

μ

i,

$$d_i = \frac{d_{i\min} + d_{i\max}}{2}$$

ρ :

μ

,

$$\rho' = \frac{\rho_F - \rho_w}{\rho_w}$$

ρ_F

ρ_w

μ

[kg/m³],

τ_{0cr}

:

μ

[N/m²],

τ_0

:

μ

[N/m²].

R_s

. 16.34

,

μ

16.1.5.

,

$R_s,$

μ 0.8

,

μ

$\mu\mu$

μ 1

IR

,

μ

μ

μ

μ

16.4.2

μ

ms

μ

$\mu\mu$

μ

μ

μ

μ

μ

μ

μ

,

$C(y)$

μ

$V(y):$

$$m_s = \int_{y=a}^{y=h} C(y) \cdot V(y) \cdot dy \quad (16.36)$$

μ

:

$$C: \left[\frac{\text{kg}}{\text{m}^3} \right], \quad V: \left[\frac{\text{m}}{\text{s}} \right] \quad \text{και} \quad m_s: \left[\frac{\text{kg}}{\text{m} \cdot \text{s}} \right]$$

$h[\text{m}]$

,

$a [\text{m}]$

μ

μ

μ
(. 16.9).

$C(y)$

μ

,

,

μ

μ

μ

μ

μ

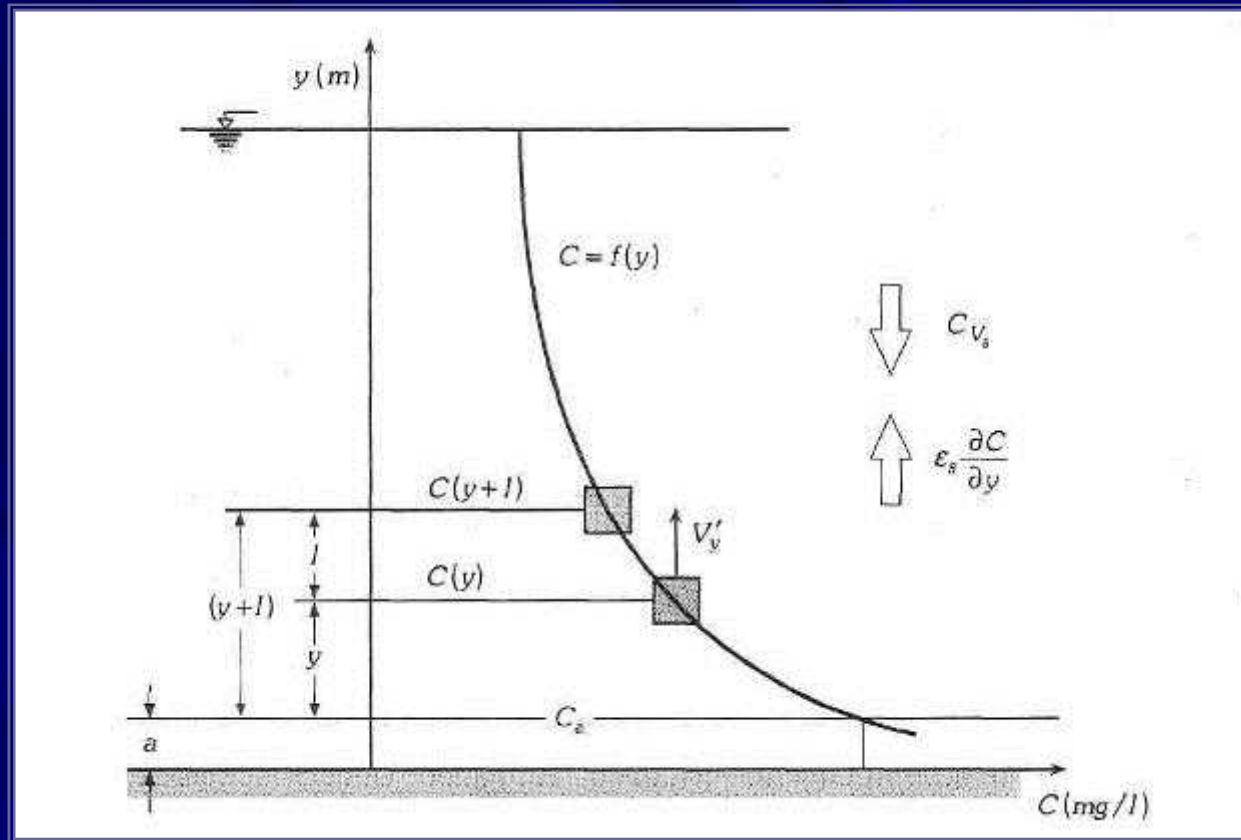
μ

,

μ

μ , μ μ , μ
 μ , μ . y , μ
 μ , μ , μ , μ
 $y + l$ y μ ,

C μ / μ



. 16.9:

(Vetter, 1992)

μ μ $y + l.$ μ
 μ μ $($ $)$ Vs.

$$V_0 C + \epsilon_s \frac{dC}{dy} = 0, \quad (16.37)$$

$$\epsilon_s = \beta \epsilon_m \quad (\text{Rouse, 1937}) \quad (16.38)$$

$$\epsilon_m = V_0^* K y \frac{h-y}{h} \quad (16.39)$$

(: Von Karman).

16.37

μ

16.38

16.39

$$\frac{C}{C_s} = \left(\frac{h-y}{y} \frac{a}{h-a} \right)^z, \quad (\text{Rouse, 1937}) \quad (16.40)$$

z

:

$$z = \frac{V_s}{\beta K V_o^*} \quad (16.41)$$

16.10

μ

μ

μ

a

μ

z . Ca

μ

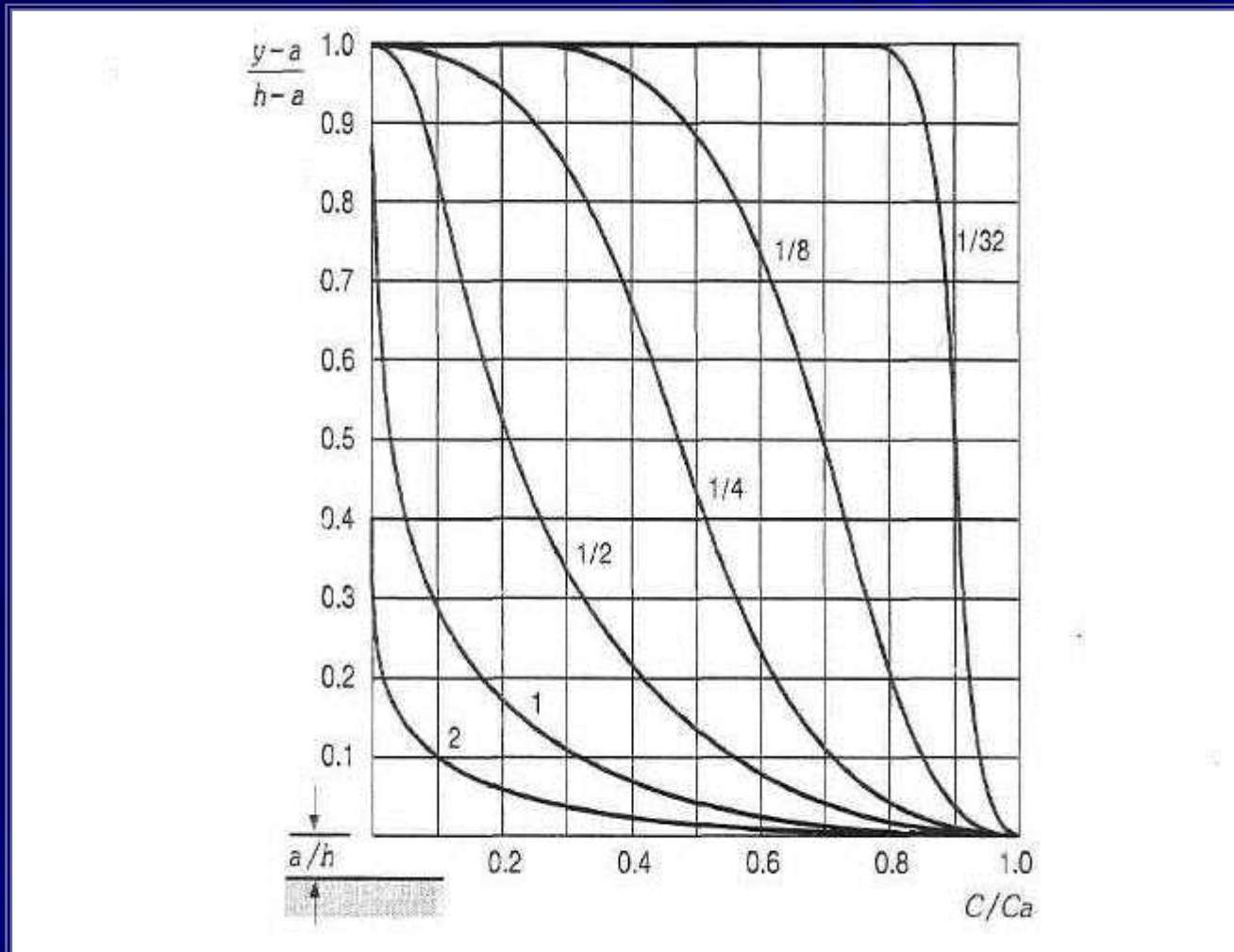
μ

μ

16.37.

μ

μ



. 16.10:

μ

μ

μ

16.4.3

(Vetter, 1992):

(
(1950).

Einstein

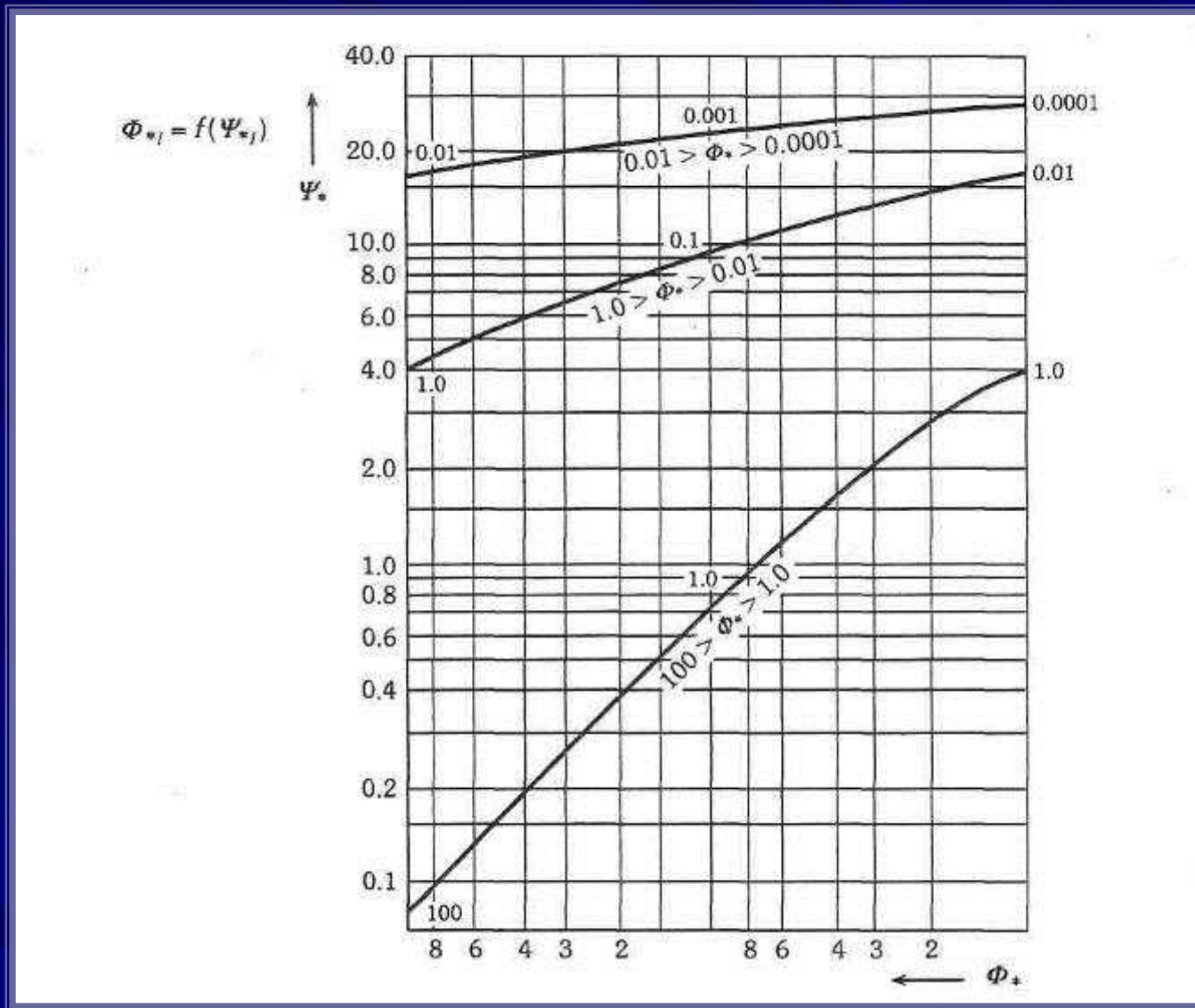
$$p_i = \frac{A_{*i} \Phi_{*i}}{1 + A_{*i} \Phi_{*i}} = 1 - \sqrt{\pi} \int_{-B_{*i} \Psi_{*i} - \frac{1}{\pi_0}}^{B_{*i} \Psi_{*i} - \frac{1}{\pi_0}} e^{-t^2} dt \quad (16.42)$$

W_b (qGi , Einstein, [N/m · s])
 F_L W_b/F_L

$$qGi = \Phi_{*i} \rho_l \rho_F g^{3/2} d_i^{3/2} \rho^{1/2} \quad (16.43)$$

. 16.42 Einstein
 $\mu = 27.0, = 0.156 \quad 1/n_0 = 2.0.$
 . 16.12.
 $= f () \mu$
 (. . Shulits Hill, 1968).

. . DVWK, 1988).
 :



. 16.12:

= f()

Einstein (1950)

$$\Psi = \rho' \frac{d}{R'I} \quad (16.44)$$

d : μ [m],
 ρ' : μ [-],
 R' : μ , [m],
 (. 16.1.5).

μ μ μ . 16.36,
 μ μ μ Rouse (1937)
 μ μ μ Keulegan (1938).
 μ μ μ z (. 16.41),
 μ μ μ μ μ (. 16.1.5).
 μ μ μ μ μ μ μ μ
 μ [N/m s],
 μ [N/m³]:

$$q_{st} = 11.6 V_0^* \cdot C_a a \left[2.3 \log \left(30.2 \frac{h \cdot x}{k_s} \right) I_{1i} + I_{2i} \right] \quad (16.45)$$

$$I_{1i} = 0.216 \frac{n_{ai}^{z_i-1}}{(1-n_{ai})^{z_i}} \int_{n_{ai}}^1 \left(\frac{1-n}{n} \right)^{z_i} dn \quad (16.46)$$

$$I_{2i} = 0.216 \frac{n_{ai}^{z_i-1}}{(1-n_{ai})^{z_i}} \int_{n_{ai}}^1 \left(\frac{1-n}{n} \right)^{z_i} \ln n \, dn \quad (16.47)$$

$$n = y/h$$

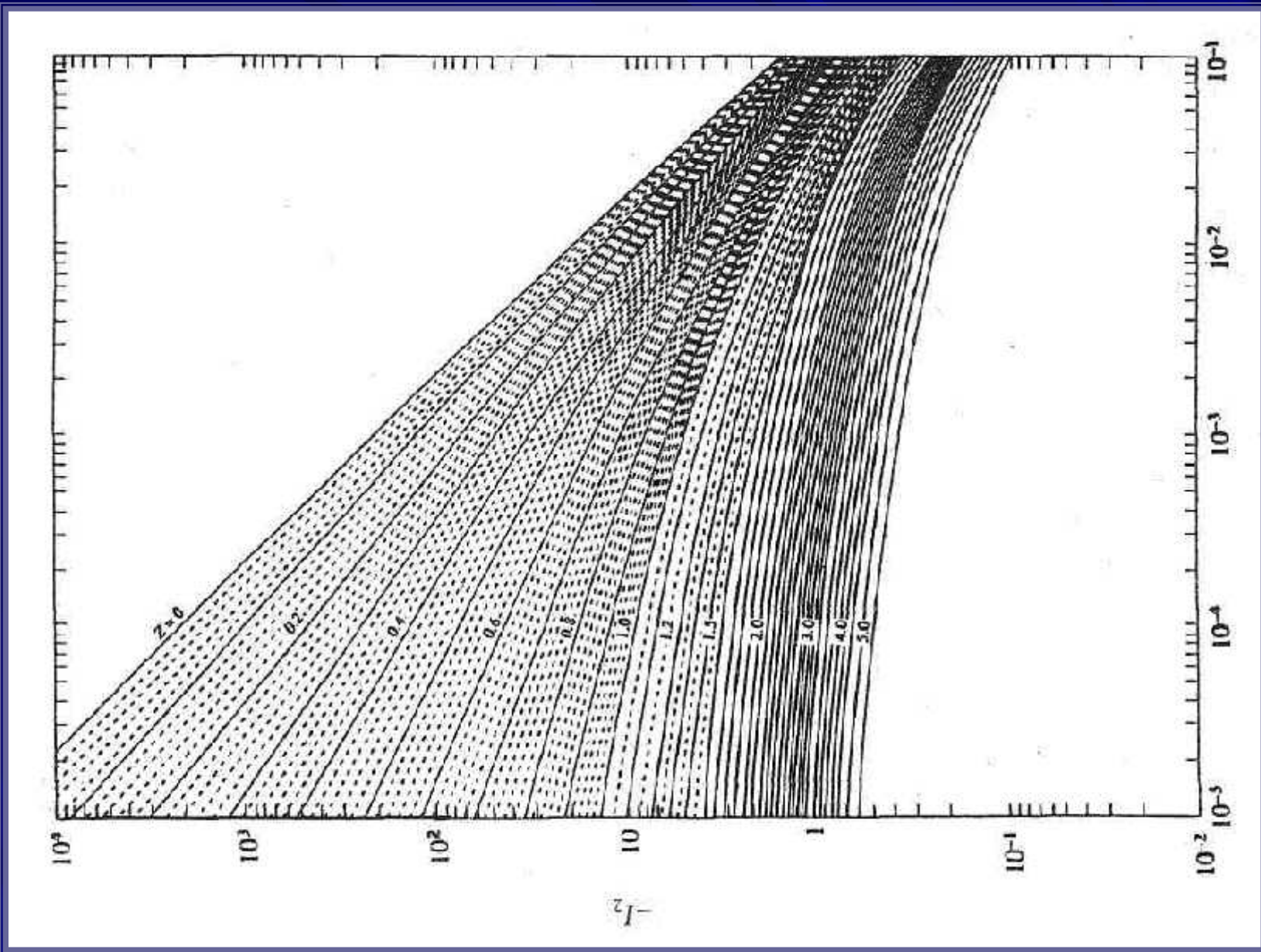
$$n_{ai} = \frac{2d_i}{h}, \quad \text{όπου} \quad d_i = \sqrt{d_{i\max} \cdot d_{i\min}} \quad (16.48)$$

$$z_i = \frac{V_{st}}{0.4 V_0^*} \quad (16.49)$$

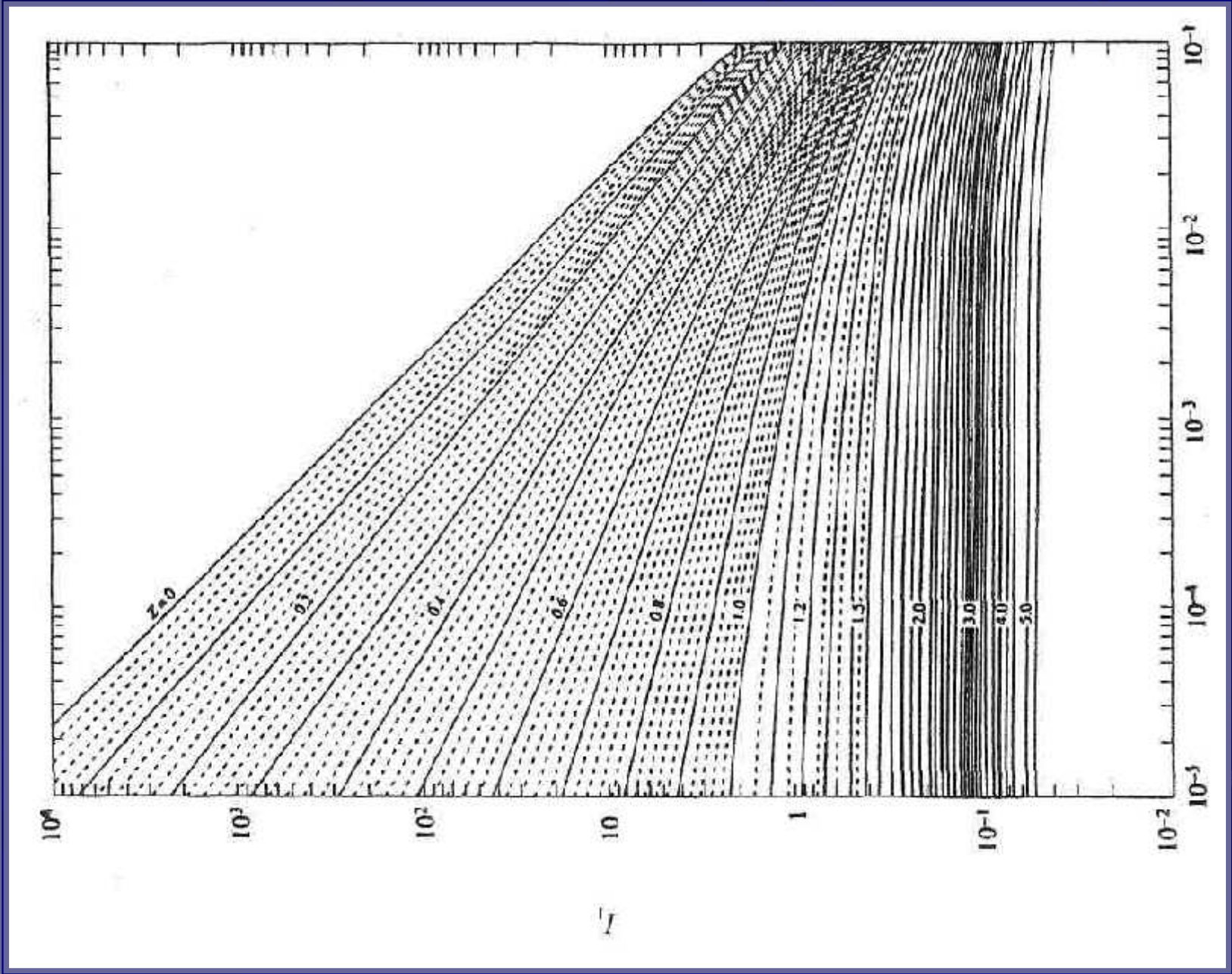
16.47μ , 16.46μ , 16.13 , 16.14
 Simpson.
 $[N/m \cdot s]$

$$q_{Fi} = q_{Gi} (P I_{1i} + I_{2i} + 1) \quad (16.50)$$

$$P = 2.3 \log \left(30.2 \frac{hX}{k_s} \right)$$



Σκ. 16.14: Ολοκλήρωμα I_2 (Einstein) ως συνάρτηση των n_2 και z .



Σχ. 16.13: Ολοκλήρωμα Γ_1 (Einstein) ως συνάρτηση των η_p και z .

Einstein (bed material layer) $a = 2d$,
 Karim Model). Kennedy (1983), TLTM (Total Load Transport Model).
 q_F [m³/s » m] V_m
 [m/s],

$$\log \frac{q_F}{\sqrt{g\rho' d_{50}^3}} = -2.2786 + 2.9719 x_1 + 0.2989 x_2 x_6 + 1.06 x_1 x_6 \quad (16.52)$$

$$\log \frac{V_m}{\sqrt{g\rho' d_{50}}} = 0.9045 + 0.1665 x_8 + 0.0831 x_4 x_5 x_8 + 0.2166 x_4 x_5 - 0.0411 x_2 x_3 x_4 \quad (16.53)$$

:

$$x_1 = \log V_1, x_2 = \log V_2, \dots, x_8 = \log V_8 \quad (16.54)$$

$$V_1 = \frac{V_m}{\sqrt{g\rho' d_{50}}}, \quad V_2 = \frac{h}{d_{50}}, \quad V_3 = I \cdot 10^3, \quad V_4 = \frac{V_0^*}{V_s} \quad (16.55)$$

$$V_5 = \frac{V_s d_{50}}{v}, \quad V_6 = \frac{V_0^* - V_{0cr}^*}{\sqrt{g\rho' d_{50}}}, \quad V_8 = \frac{q_F}{\sqrt{g\rho' d_{50}^3}} \quad (16.56)$$

$$V_{0cr}^* : \mu \quad [m/s],$$

$$\mu \quad h \quad q_F \quad \mu \quad V_m \quad V_m \quad , \quad \mu \quad \mu \quad q_F$$

Engelund Hansen (1967)

$$f_{EH} \Phi = 0.1 \theta^{5/2} \quad (16.57)$$

$$m_F = \Phi \rho_F \sqrt{\rho' g d^3} \quad (16.58)$$

$$f_{EH} = \frac{2l}{F_r} = \frac{2ghl}{V_m^2} \quad (16.59)$$

$$\theta = \frac{\tau_0}{\rho_w g \rho' d} = \frac{hl}{\rho' d} \quad (16.60)$$

(l: μ , Fr: μ Froude).

μ

V_m

:

$$V_m = V_0^{*'} \left(6.0 + 2.5 \ln \frac{h'}{k_s} \right) \quad (k_s = 2.5 d) \quad (16.61)$$

Engelund - Hansen,

Einstein (16.1.5),

μ

($V_0^{*'} = \sqrt{gh'I}$), $h' = \frac{\theta'}{\theta} \cdot h$, όπου $\theta' = 0.06 + 0.4\theta^2$ ή $\theta' = 0.4\theta^2$, όταν $\theta > 0.15$

$$V_0^{*'} = \sqrt{gh'I} \quad (16.62)$$

$$h' = \frac{\theta'}{\theta} \cdot h, \quad (16.63)$$

$$\text{όπου } \theta' = 0.06 + 0.4\theta^2 \quad (16.64)$$

$$\text{ή } \theta' = 0.4\theta^2, \text{ όταν } \theta > 0.15 \quad (16.65)$$

Yang (1973, 1979)

Yang
 power), V_{mb} " (unit stream
 CF [mg/l]

$$\frac{V_m I}{V_s} - \frac{V_{mer} I}{V_s} :$$

$$\log C_F = 5.435 - 0.286 \log \frac{V_s d_{50}}{v} - 0.457 \log \frac{V_0^*}{V_s} +$$

$$+ \left(1.799 - 0.409 \log \frac{V_s d_{50}}{v} - 0.314 \log \frac{V_0^*}{V_s} \right) \cdot$$

$$\log \left(\frac{V_m I}{V_s} - \frac{V_{mer} I}{V_s} \right), \quad (16.66)$$

V_s : [m/s],
 V_{mcr} : μ μ [m/s].
 :

Yang

$$\frac{V_{mcr}}{V_s} = \frac{2.5}{\log\left(\frac{V_0^* d_{50}}{\nu}\right) - 0.06} + 0.66, \quad \text{όταν} \quad 0 < \frac{V_0^* d_{50}}{\nu} < 70 \quad (16.67)$$

$$\frac{V_{mcr}}{V_s} = 2.05, \quad \text{όταν} \quad \frac{V_0^* d_{50}}{\nu} \geq 70 \quad (16.68)$$

m_F [kg/m s]

:

$$m_F = C_F \cdot 0.001 \cdot h \cdot V_m \quad (16.69)$$

μ Yang (1979) μ
 μ μ , μ μ
 μ μ :

$$\log C_F = 5.165 - 0.153 \log \frac{V_s d_{50}}{\nu} - 0.297 \log \frac{V_0^*}{V_s} +$$

$$+ \left(1.780 - 0.360 \log \frac{V_s d_{50}}{\nu} - 0.480 \log \frac{V_0^*}{V_s} \right) \log \frac{V_m I}{V_s} \quad (16.70)$$

Zanke (1982)

$$q_G \left[\frac{\text{m}^3}{\text{m} \cdot \text{s}} \right] = \frac{1}{p} \cdot 6.36 \cdot 10^{-4} \left(\frac{V_0^{*2} - V_{0cr}^{*2}}{V_s^2} \right) D^{*4} v$$

$$q_s \left[\frac{\text{m}^3}{\text{m} \cdot \text{s}} \right] = \frac{1}{p} \cdot 6.36 \cdot 10^{-5} \cdot \frac{h}{h_1} \cdot \frac{(V_0^{*2} - V_{0cr}^{*2})(V_0^{*2} - V_{0\ell}^{*2})}{V_s^4} D^{*4} v \left(\frac{v}{V_0 - v} \right)^{1/4}$$

40% Zanke, V_s [m/s]

$$V_{0\ell}^* = 0.4 V_s \quad (16.73)$$

$$V_{01}^* = 0.27 (\rho' g d_{50})^{1/2} \quad (16.76)$$

D^* μ d_{ch} [m]: μ

$$D^* = \left(\frac{\rho' g}{\nu^2} \right)^{1/3} \cdot d_{ch} \quad (16.74)$$

μ :

=0.7,

$\nu = 1.78 \cdot 10^{-6} \text{ m}^2/\text{s}$, μ 0°C ,

$h_1 = 0.01 \text{ m}$.

μ

:

$$V_{0cr}^* = V_{01}^* + V_{02}^* - (V_{01}^* \cdot V_{02}^*)^{1/2} \quad (16.75)$$

:

$$V_{01}^* = 0.27 (\rho' g d_{50})^{1/2} \quad (16.76)$$

$$V_{02}^* = 0.5 (\rho' g \nu)^{1/3} \quad (16.77)$$

$$q_F = q_G + q_s \quad (16.78)$$

$$m_F = q_F \cdot \rho_F \cdot p \quad (16.79)$$

van Rijn (1984),

$$T^* = \frac{V_0^{*2} - V_{0cr}^{*2}}{V_{0cr}^{*2}}$$

$$T^* = \frac{V_0^{*2} - V_{0cr}^{*2}}{V_{0cr}^{*2}} \quad (16.80)$$

van Rijn,

Einstein,

$$a \quad (a = k_s = 3 d_{90})$$

μ

Einstein,

Ca.

μ μ (μ)

μ , μ van Rijn
" (. 16.4.2)

, μ van Rijn μ
μ μ . μ

μ μ van Rijn (1984).

16.4.4

μ

μ

μ 1

μ μ

:

- $b = 45.0 \text{ m}$
- $h = 3.5 \text{ m}$
- $V_m = 2.10 \text{ m/s}$
- $l = 6.5$
- $k_{st} = 38.0 \text{ m}^{1/3}/\text{s}$
- :
- $d_{90} = 7.9 \text{ cm}$
- $d_{50} = 1.2 \text{ cm}$
- $\rho_F = 2650 \text{ kg/m}^3$

μ

μ

μ

.

μ

) μ μ μ
) μ μ μ

Meyer - Peter
Einstein.

Muller

)
Muller.

μ μ

. 16.34
 μ :

Meyer-Peter

$$g = 9.81 \text{ m/s}^2$$

$$\rho_w = 1000 \text{ kg/m}^3$$

$$\rho' = \frac{\rho_F - \rho_w}{\rho_F} = \frac{2650 - 1000}{1000} = 1.65$$

$$k_T = \frac{26}{\sqrt[6]{d_{90}}} = \frac{26}{\sqrt[6]{0.079}} = 39.7 \text{ m}^{1/3}/\text{s}$$

$$I_R = \left(\frac{k_{st}}{k_T} \right)^{3/2} I = \left(\frac{38.0}{39.7} \right)^{3/2} \times 6.5 \times 10^{-4} = 6.087 \times 10^{-4}$$

R_s μ μ μ

Einstein Barbarossa (1952):

$$A = R_w U_w + R_s U_s \quad (16.81)$$

$$R_w = \left(\frac{V_m}{k_w I^{0.5}} \right)^{1.5} \quad (16.82)$$

. 16.81 16.82 :

$$R_s = \frac{A - \left(\frac{V_m}{k_w I^{0.5}} \right)^{1.5} U_w}{U_s} \quad (16.83)$$

$$w = \frac{R^2 U}{k_w} \quad (16.2)$$

$$k_w = k_{st} = 38.0 \text{ m}^{1/3}/\text{s}$$

$$R_5 = 3.0 \text{ m}$$

$$d_{50} = 0.012 \text{ m}$$

$$U_w = 3.5 + 3.5 = 7.0 \text{ m/s}$$

$$U_5 = 45.0 \text{ m/s}$$

$$V_m = 2.10 \text{ m/s}$$

$$= 6.5$$

$$d_m (16.34)$$

$$= 16.83$$

$$\Psi' = 1.65 \times \frac{0.012}{3.0 \times 6.5 \times 10^{-4}} = 10.15$$

=8.3. μ . 16.12, = f(), μ μ

μ μ , . 16.43 $Pi = 1.0$.
 μ ,
 :

$$q_G = \Phi_{Pr} g^{3/2} d_{50}^{3/2} \rho^{1/2}$$

\dot{n}

$$q_G = 8.3 \times 10^{-2} \times 2650 \times 9.81^{3/2} \times 0.012^{3/2} \times 1.65^{1/2} = 11.41 \frac{N}{m \cdot s}$$

$$\text{Επομένως } m_G = \frac{11.41}{9.81} = 1.16 \frac{kg}{m \cdot s}$$

μ μ , μ μ R' μ μ R' R'' ,
 16.1.5), (.

$\frac{\mu}{2}$

0.00038μ 2650 kg/m^3 4.6 m $d_{65} = 0.75 \text{ mm}$ $d_{35} = 0.5 \mu$
 mm. $1.01 \text{ m}^2/\text{s.}$ R'
 $R''.$

$o = o' + o''$ Vm $. 16.18,$

$$\rho_w g R I = \rho_w g R' I + \rho_w g R'' I \quad (16.85)$$

$$R = R' + R'' \quad (16.86)$$

R $h = 4.6 \text{ m}$ $(h: \mu)$ μ, μ μ μ

R' R'' Einstein. μ
 R' μ $V_0^{*'} \mu$ $4.6 \text{ m} (1 \mu)$ μ
 $:$

$$V_0^{*'} = \sqrt{gR'I} = \sqrt{9.81 \times 4.6 \times 0.00038} = 0.131 \text{ m/s}$$

:

$$\delta' = \frac{11.6 \nu}{V_0^{*'}} = \frac{11.6 \times 1.01 \times 10^{-6}}{0.131} = 8.94 \times 10^{-5} \text{ m}$$

Σχηματίζουμε τον λόγο $\frac{k_s}{\delta'} = \frac{d_{65}}{\delta'} = \frac{0.75 \times 10^{-3}}{8.94 \times 10^{-5}} = 8.39.$

$\mu\mu$ μ μ k_s / μ μ
 16.4.3. $x,$
 (White, Milli $\mu\mu, \mu,$
 Crabbe, 1973). μ :

$$2.35 \leq \frac{d_{65}}{u} < 10$$

:

$$x = 0.926 \left| \log \frac{d_{65}}{\delta'} - 1 \right|^{2.43} + 1.0 \quad (16.87)$$

\hat{n}

$$x = 0.926 \left| \log 8.39 - 1 \right|^{2.43} + 1.0 = 1.0$$

$$V_m = V_0^{*'} * 5.75 \log \left(12.27 \frac{R' x}{k_s} \right) \quad (16.88)$$

$$V_m = 0.131 \times 5.75 \log \left(12.27 \frac{4.6 \times 1.0}{0.75 \times 10^{-3}} \right) = 3.67 \text{ m/s}$$

$$\Psi' = \rho' \frac{d_{35}}{R' I} = 1.65 \frac{0.5 \times 10^{-3}}{4.6 \times 0.00038} = 0.472$$

(Shulits

Hill, 1968).

$$\frac{V_m}{V_0^{*''}} = 40.0 \Psi'^{-1.288} \quad (16.89)$$

ή

$$\frac{3.67}{V_0^{*''}} = 40.0 \times 0.472^{-1.288},$$

οπότε $V_0^{*''} = 0.0349 \text{ m/s}$

Αλλά $V_0^{*''} = \sqrt{gR''I}$ ή $0.0349 = \sqrt{9.81 \times R'' \times 0.00038}$,

οπότε $R'' = 0.327 \text{ m}$.

Ως γνωστό, $R = R' + R''$ ή $R = 4.6 + 0.327 = 4.927 \text{ m} \approx 4.93 \text{ m}$.

μ 4.93 m

μ 4.6 m

μ

μ μ , μ
μ μ

μ μ
μ

, μ μ
μ μ
:

μ 2:

$$R' = 4.0 \text{ m}$$

$$V_0^* = 0.122 \text{ m/s}$$

$$\delta' = 9.60 \times 10^{-5} \text{ m}$$

$$k_s/\delta' = 7.81$$

$$x = 1.0$$

$$V_m = 3.38 \text{ m/s}$$

$$\Psi' = 0.543$$

$$V_0^{*''} = 0.038 \text{ m/s}$$

$$R'' = 0.387 \text{ m}$$

$$R = 4.39 \text{ m}$$

Δοκιμή 3:

$$R' = 4.3 \text{ m}$$

$$V_0^* = 0.127 \text{ m/s}$$

$$\delta' = 9.22 \times 10^{-5} \text{ m}$$

$$k_s/\delta' = 8.13$$

$$x = 1.0$$

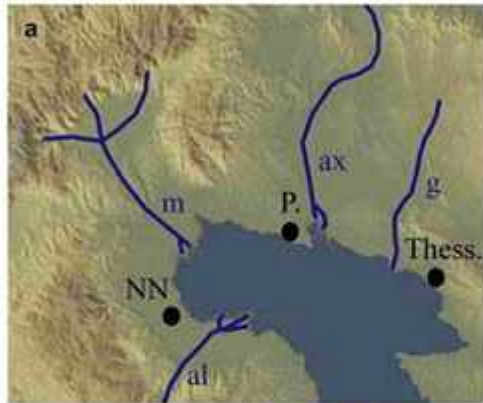
$$V_m = 3.54 \text{ m/s}$$

$$\Psi' = 0.505$$

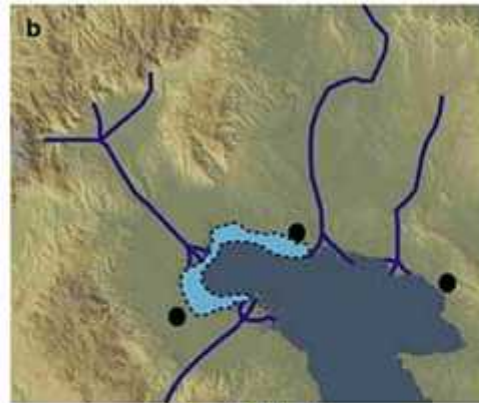
$$V_0^{*''} = 0.037 \text{ m/s}$$

$$R'' = 0.367 \text{ m}$$

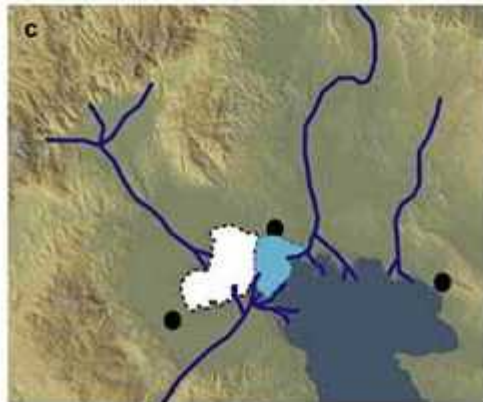
$$R = 4.67 \text{ m}$$



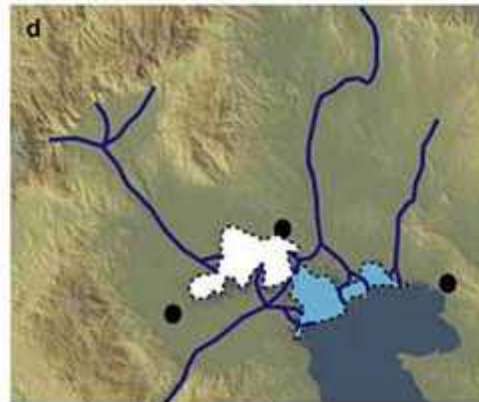
Νεολοθική εποχή ως 3.000 π.χ.



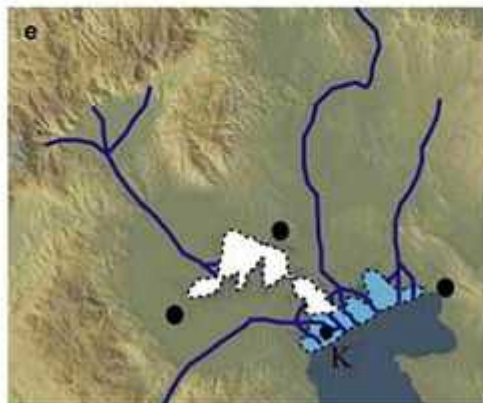
Εποχή Χαλκού



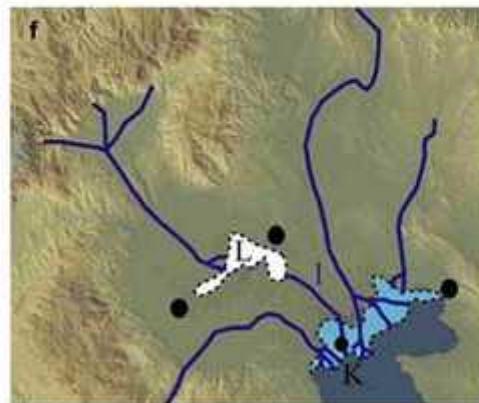
Ύστερη εποχή Χαλκού



Αρχαϊκή και Κλασσική περίοδος



Ρωμαϊκή εποχή



400 μ.Χ. έως 1908 μ.Χ.

Ποταμοί:
 m Μογλενίτσας
 al Αλιάκμονας
 ax Αξιός
 g Γαλλικός
 l Λουδίας

Πόλεις:
 NN. Νέα Νικομήδεια
 (νεολιθική)
 P. Πέλλα (5ος αι. π.Χ.)
 K. Κλειδί (3ος αι. μ.Χ.)

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